

Generalised method for the determination of heterogeneous batch distillation regions

Lang P. and G. Modla

Budapest University of Technology and Economics, Department of Process Engineering,
H-1521 Budapest, Muegyetem rkp. 3-5, lang@vegyelgep.bme.hu

Abstract

A new, general method for the calculation of residue curves and for the determination of batch distillation regions of heteroazeotropic distillation is suggested. The method proposed, which means the extension of the method of Pham and Doherty, takes into consideration the possibility of the withdrawal of any fraction of either liquid phase from the decanter as distillate. The simplified and rigorous simulation calculations were carried out for the mixtures dichloromethane-acetone (low a) + water (heavy, selective, heterogeneous entrainer), water-ethylenediamine (maximum azeotrope) + benzene (light, selective, heterogeneous entrainer) and isopropanol-water (minimum azeotrope) + benzene (light, nonselective, heterogeneous entrainer). The new method gives the right sequence of the cuts for all operation modes and strategies of heterogeneous batch distillation.

Keywords: Batch Distillation, Heterogeneous Entrainer, Separation of Azeotropes, Residue Curves

References

- Bernot C., M. Doherty, M. and M. F. Malone, (1990). Patterns of composition change in multicomponent batch distillation, *Chemical Engineering Science*, **45**, 1207.
- Bril Zs. A., Mozzsuhin, A. C., Petljuk and F. B., Serafimov, L. A., (1974). Mathematical modelling of the rectification of multicomponent mixtures with liquid phase splitting on the plates of the column, *Teor. Osn. Chim. Technol.*, **8**, 351.
- Chemstations, (2005). "CHEMCAD User Guide".
- Doherty, M. F. and J. D. Perkins, (1978). On the Dynamics of Distillation Processes I. The Simple Distillation of Multicomponent Nonreacting, Homogeneous Liquid Mixtures, *Chemical Engineering Science*, **33**, 281.
- Doherty M. F., and G. A. Calderola, (1985). Design and Synthesis of Homogeneous Azeotropic Distillations. 3. The Sequencing of Columns for Azeotropic and Extractive Distillation", *Industrial Engineering Chemistry Fundamentals* **24**, 474.
- Ewell, R. H. and L. M. Welch, (1945). Rectification in Ternary Systems Containing Binary Azeotropes, *Industrial Engineering Chemistry*, **37**, 1224.
- Kiva V., E. Hilmen and S. Skogestad, (2003). Azeotropic Phase Equilibrium Diagrams: a Survey, *Chemical Engineering Science*, **58**, 1903-1953.
- Koehler, J., H. Haverkamp, and N. Schadler, (1995). Zur Diskontinuierlichen Rektifikation Azeotroper Gemische mit Hilfsstoffeinsatz, *Chemie Ingenieur Technik*, **67** (8), 967.
- Matsuyama, H., Nishimura, H., (1977). Topological and thermodynamic classification of ternary vapor-liquid equilibria. *Journal of Chemical Engineering of Japan*, **10** (3), 181.
- Modla G., P. Lang , B. Kotai and K. Molnar, (2003). Batch Heteroazeotropic Rectification of a Low Relative Volatility Mixture under Continuous Entrainer Feeding, *AIChE Journal*, **49** (10), 2533.

Chem. Eng. Sci., 61, 4262-4270 (2006).

- Pham, H. N. and M. F. Doherty, (1990). Design and synthesis of heterogeneous azeotropic distillations II. Residue curve maps, *Chemical Engineering Science*, **45** (7), 1837.
- Rodriguez-Donis I, V. Gerbaud and X. Joulia, (2002). Feasibility of Heterogeneous Batch Distillation Processes, *AICHE Journal*, **48** (6), 1168.
- Rodriguez-Donis Y., J. A. Equijarosa, V. Gerbaud and X. Joulia, (2003). Heterogeneous Batch-extractive Distillation of Minimum Boiling Azeotropic Mixtures, *AICHE Journal*, **49** (12), 3074.
- Serafimov, L.A. (1970). The Azeotropic Rule and the Classification of Multicomponent Mixtures. VII. Diagrams for Ternary Mixtures. *Russian Journal of Physical Chemistry* **44** (4), 567.
- Skouras S., V. Kiva and S. Skogestad, (2005a). Feasible separations and entrainer selection rules for heteroazeotropic batch distillation, *Chemical Engineering Science*, **60**, 2895.
- Skouras S., S. Skogestad and V. Kiva, (2005 b). Analysis and Control of Heteroazeotropic Batch Distillation, *AICHE Journal*, **51** (4), 1144-1157.